

Q1 ARASH
Problem #1

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Convert to correct units to be able to look up closest values in steam tables in back of text.

a) 10 MPa $0.003 \text{ m}^3/\text{kg} = 3 \text{ cm}^3/\text{g}$
wet steam

b) 200°C $0.1 \text{ m}^3/\text{kg} = 100 \text{ cm}^3/\text{g}$
wet steam

c) 2200 kPa 3134 kJ/kg
superheated steam

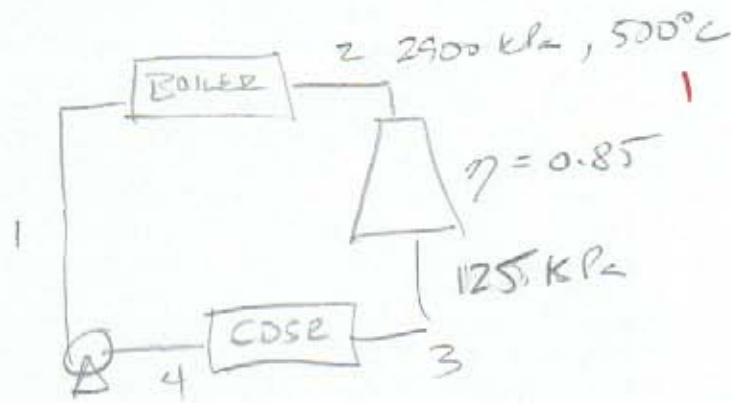
d) 300°C 10 MPa
subcooled liquid

e) 5°C , $147.2 \text{ m}^3/\text{kg}$
saturated vapour.

7 minutes

10:35
24 min

Q2) ARASHI



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Constant Turbine

$$H_2 = 3457.3 \text{ kJ/kg} \quad 2$$

$$S_2 = 7.2512 \text{ kJ/kg K}$$

Isentropic

$$S_3 = S_2 = 7.2512 \text{ kJ/kg K} \quad 1$$

125 kPa

$$H_{125}^L = 444.356 \text{ kJ/kg} \quad 2$$

$$S_{125}^L = 1.3740 \text{ kJ/kg K}$$

$$H_{125}^V = 2685.2 \text{ kJ/kg} \quad 2 \quad 3$$

$$S_{125}^V = 7.2847 \text{ kJ/kg K}$$

$$(x_3)_s = \frac{7.2512 - 1.3740}{7.2847 - 1.3740} = 0.9943$$

$$H_3 = 3457.3 + 0.85 \left([0.994 \cdot 2685.2] + (1 - 0.994)(444.356) - 3457.3 \right)$$

$$= 3457.3 + 0.85 (-786.8)$$

$$= 2788.5 \text{ kJ/kg} \quad 1$$

$$W_t = \Delta H_t = -668.8 \text{ kJ/kg} \quad 3$$

Q2

p2

Consider Pump.

$$H_4 = H_{125 \text{ kPa}}^L = 444.356 \text{ kJ/kg.}$$

$$(\Delta H)_s = W_p = V \Delta P = 1.049 (\text{L/kg}) (2900 - 125) \text{ kPa} \\ = 2,911.5 \text{ J/kg} = 2.91 \text{ kJ/kg}$$

$$\Delta H = \frac{(\Delta H)_s}{\eta} = \boxed{3.43 \text{ kJ/kg.} = W_p} \quad 3$$

$$H_1 = H_4 + \Delta H = 444.356 + 3.43 \quad | \\ = 447.78 \text{ kJ/kg}$$

Consider Boiler

$$\Delta H = Q_H = H_2 - H_1 = (3457.3 - 447.78) \\ \boxed{Q_H = 3009.52 \text{ kJ/kg.}} \quad 2$$

Plant Efficiency

$$\eta = \frac{|W_{t1}| - |W_{p1}|}{Q_H} = \frac{668.8 - 3.43}{3009.52} \quad | \\ = 0.221 \quad 3$$

The plant is 22.1% efficient.

Q3 / PROSHAD

(i) Energy content of fuel

$$E_{\text{fuel}} = 171,000 \text{ L} \times 34.8 \text{ MJ/L} \\ = 5,950,800 \text{ MJ}$$

(ii)

$$\eta = \frac{\eta_t \eta_c (T_c/T_A)(1 - 1/\alpha) - (\alpha - 1)}{\eta_c (T_c/T_A - 1) - (\alpha - 1)}$$

$$\alpha = \left(\frac{P_B}{P_A}\right)^{\frac{\gamma-1}{\gamma}} = 34.4 \left(\frac{1.4-1}{1.4}\right) = 2.748$$

$$T_c/T_A = \frac{(1700 + 273.15)}{(-54 + 273.15)} = 9.004$$

$$\eta = \frac{(0.85)(0.9)(9.004)(1 - 1/2.748) - (2.748 - 1)}{[0.9(9.004 - 1) - (2.748 - 1)]}$$

$$= 0.483$$

$$(iii) \text{ Time in air} = \frac{14,260 \text{ km}}{900 \text{ km/h}} = 15.84 \text{ hrs} \\ = 57,040 \text{ s}$$

$$\text{Power per Engine} = \frac{(0.483)(5,950,800) \text{ MJ}}{2(57,040 \text{ s})} \\ = 25.2 \text{ MW}$$

Q9) If a 40 L tank of hydrogen is pressurized to 5000 psi (1 bar = 14.5038 psia) at 25°C how many kilograms of hydrogen are stored in the tank? Use the appropriate equation of state. According to the IGL how many kilograms would be stored?

H_2 molar mass = 2.016
 $\omega = -0.216$
 $T_c = 33.19 \text{ K}$
 $P_c = 13.13 \text{ bar}$

15 mm.

Given: $V_{tot} = 40 \text{ L}$
 $P = 5000 \text{ psi} = 344.7 \text{ bar}$
 $T = 25^\circ\text{C} = 298.15 \text{ K}$

Since $T_r > 4.0$ use Pitzer correlations 2

$$B^0 = 0.083 - \frac{0.422}{T_r^{1.6}} \quad B^1 = 0.139 - \frac{0.172}{T_r^{4.2}}$$

$$Z = 1 + B^0 \frac{P_r}{T_r} + \omega B^1 \frac{P_r}{T_r}$$

$$P_r = \frac{344.7}{13.13} = 26.26 \quad T_r = \frac{298}{33.19} = 8.98 \quad 2$$

$$B^0 = 0.07041$$

$$B^1 = 0.1390$$

$$Z = 1 + 0.7041 \left(\frac{26.26}{(8.98)^{1.6}} \right) + (-0.216) \left(\frac{26.26}{(8.98)^{4.2}} \right)$$

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P2

$$z = 1.181 \quad \checkmark$$

$$PV = zRT$$

$$V = \frac{zRT}{P} = \frac{(1.181) \left(8.314 \frac{\text{L} \cdot \text{kPa}}{\text{mol} \cdot \text{K}} \right) (298 \text{ K})}{34,474 \text{ kPa}}$$

$$= 0.0804 \text{ L/mol} \quad \checkmark$$

$$n = \frac{V_{\text{tot}}}{V} = \frac{40 \text{ L}}{0.0804 \text{ L/mol}} = 497.8 \text{ mol} \quad \checkmark$$

$$m = 2.0179 \frac{\text{g}}{\text{mol}} \times 497.8 \text{ mol} = 1003.5 \text{ g} \\ = 1.004 \text{ kg} \quad \checkmark$$

b) IGL

$$PV = nRT$$

$$PV = \frac{m}{M} RT$$

$$m = \frac{MPV}{RT} = \frac{(2.017 \text{ g/mol}) (34,473 \text{ kPa}) (40 \text{ L})}{\left(8.314 \frac{\text{L} \cdot \text{kPa}}{\text{mol} \cdot \text{K}} \right) (298 \text{ K})}$$

$$= 1.12 \text{ kg}$$

Q5) CHEE 210 WINTER 2010
PROSHAD



$$C_p = \frac{11}{2} R \quad C_v = C_p - R = \frac{9}{2} R$$

$$\gamma = \frac{11}{9} = 1.222$$

Reversible Adiabatic.

$$\frac{T_2}{T_1} = \left(\frac{P_2}{P_1}\right)^{\frac{R}{C_p}} \quad T_2 = T_1 \left(\frac{P_2}{P_1}\right)^{\frac{R}{C_p}}$$

$$T_2 = (300) \left(\frac{8}{1.1}\right)^{\frac{2}{11}} = 430.3 \text{ K}$$

$$(\Delta H)_s = \frac{11}{2} R (430.3 - 300) = 5959 \text{ kJ}$$

$$\Delta H = \frac{11}{2} R (480 - 300) = 8231 \text{ kJ}$$

$$\eta = \frac{5959}{8231} = 0.724$$

Q6) Pressure

$$\begin{aligned} a) P &= 101.3 \text{ kPa} + 110.2 \text{ kPa} \\ &= 211.5 \text{ kPa} \end{aligned}$$

b) From steam table at 211.5 kPa
water boils at 122°C

c) At atmospheric pressure water boils
at 100°C

From steam tables.

$$\text{@ } 11400 \text{ kPa } \quad 650^\circ\text{C} \quad v^v = 35.733 \text{ L/kg}$$

$$v^R = v - v^s$$

for one mole of steam from IGL

$$v = \frac{RT}{P} = \frac{(8.314)(923.15)}{11400} = 0.673 \text{ L/mol}$$

$$1 \text{ kg} = \frac{1000 \text{ g}}{18.02 \text{ g/mol}} = 37.36$$

$$\begin{aligned} v^R &= 35.73 - 37.36 \\ &= -1.631 \text{ L/kg.} \end{aligned}$$

Q18) 3AP

20 min

P1

Energy Balance

$$m_1 H_1 + m_2 H_2 - m_3 H_3 = 0$$

Mass Balance $m_1 = m_2 = \frac{1}{2} m_3 = m$

$$\therefore m H_1 + m H_2 - 2m H_3 = 0$$

$$H_1 + H_2 - 2H_3 = 0$$

Energy Balance

$$\Delta S_1 + \Delta S_2 + \Delta S_3 = 0$$

$$(H_1 - H_3) + (H_2 - H_3) = 0$$

$$C_p(T - T_1) + C_p(T - T_2) = 0$$

$$T = \frac{T_1 + T_2}{2}$$

$$\begin{aligned} \Delta S &= m C_p \ln\left(\frac{T}{T_1}\right) + m C_p \ln\left(\frac{T}{T_2}\right) \\ &= m C_p \left(\ln\left(\frac{T}{T_1 T_2}\right) \right) \end{aligned}$$

Q8

$$\Delta S^{\ddagger} = 2.303 R \ln \left(\frac{Q}{T_1 T_2} \right)$$

$$= 2.303 R \ln \left(\frac{\left(\frac{T_1 + T_2}{2} \right)^2}{T_1 T_2} \right)$$